



CO₂ Reduction and Upgrading for e-Fuels Consortium

U.S. DEPARTMENT OF ENERGY

DOE Bioenergy Technologies Office (BETO) 2023 Project Peer Review **A Feasibility Study of Utilizing Electricity to Produce Intermediates from CO₂ and Biomass**

4/10/2023

Carbon Dioxide Utilization

Gary Grim

National Renewable Energy Laboratory

Project Overview

Goal: *Guide ongoing and future R&D* in CO₂ reductive utilization by defining:

- Technical Challenges
- Opportunities
- Cost Drivers
- Carbon Intensity Drivers
- Future Technical Targets
- Scaling Risks

Outcomes: (1) FY21 – Analyzed *promising bolt-on compatible CO₂ reduction pathways* to fuels or products from standalone biorefineries, (2) FY22 – Published a *comprehensive strategic plan* for achieving industrial decarbonization goals via CO₂ conversion, with inclusion of outyear technical, cost, and carbon intensity targets, and (3) FY23 – Performing integrated TEA/LCA Analysis of CO₂ conversion

Relevance to BETO/Bioenergy Industry: Identify risks and opportunities for leveraging low-cost renewable electricity to improve biorefinery carbon utilization. Directly in support of BETO-EERE goals of (1) industrial decarbonization and (2) low-carbon strategic fuels (e.g., sustainable aviation fuel)



Quad Chart – Project Details and Financials

Timeline

- Prior AOP Cycle: Oct. 1, 2018 – Sept. 30, 2020
- Current AOP Cycle: Oct. 1, 2020 – Sept. 30, 2023

	FY22 Costed	Total Award
DOE Funding		

Project Partners

- *CO₂RUE Project*: Thermo- and Electro-catalytic routes to fuels and chemicals (WBS: 2.3.1.316)
- *CO₂RUE Project*: Economics and Sustainability of CO₂ Utilization Technologies with TEA and LCA (WBS: 2.1.0.506 / 2.1.0.507)

Project Goal

Guide existing and future research and development efforts by defining key technical challenges, risks, cost/carbon intensity drivers, and future technical targets for utilizing renewable electricity and CO₂ to improve biorefinery economics and carbon utilization

End of Project Milestone

Integrate TEA/LCA models and determine key trade-offs for the CO₂ reduction field spanning different technological approaches. This will help identify and understand key decision points based on TEA and LCA implications.

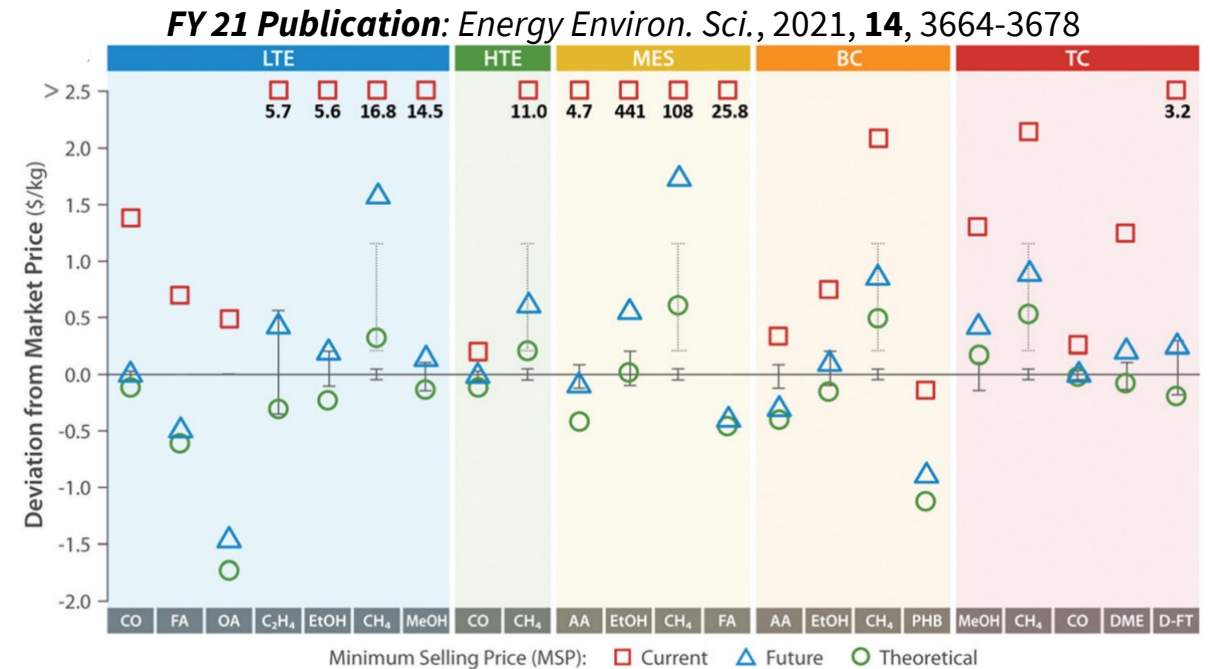
Funding Mechanism

Annual Operating Plan (AOP)



Project Overview: *Realities and Barriers of CO₂ Conversion*

- CO₂ is 73wt% O and is neither free nor pure
- CO₂ is abundant, but has no heating value
 - *Energy demand for converting CO₂ to ethylene (50% EE) is ca. >90 kWh/kg*
 - *Ammonia synthesis: ca. 8 kWh/kg*
- Transportation infrastructure is limited
- CO₂ as feedstock does not guarantee a lower carbon intensity than the incumbent



CO₂ products are expensive relative to the market

Challenge: *Overcome thermodynamic barriers to reach cost-competitive and environmentally-friendly fuels and chemicals for hard to abate sectors*



Project Overview: Many Questions on CO₂ Conversion Feasibility

Technical Feasibility

1. Relative TRL of conversion technologies?
2. What kinds of products accessible?
3. Unique advantages & disadvantages?

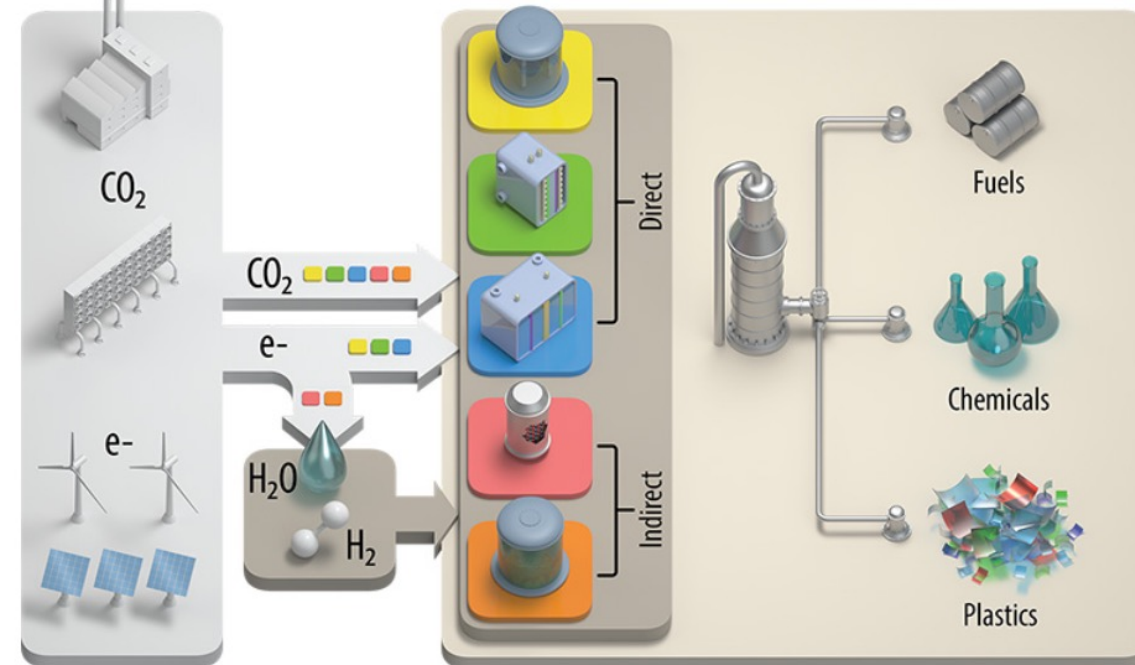
Economic Feasibility

1. What are current and future cost estimates?
2. Greatest R&D needs? Cost drivers?

Environmental Considerations

1. Carbon and energy intensity
2. Sources and footprint of energy

FY 21 Milestone: Interactive Website Launched



Opportunity: Use analysis to baseline technologies, products, and identify best practices to accelerate CO₂ utilization deployment



1. Approach

—twelve

LanzaTech

nel

AIR COMPANY

Pacific Northwest
NATIONAL LABORATORY

Argonne
NATIONAL LABORATORY



Dioxide Materials™
The CO₂ Recycling Company™

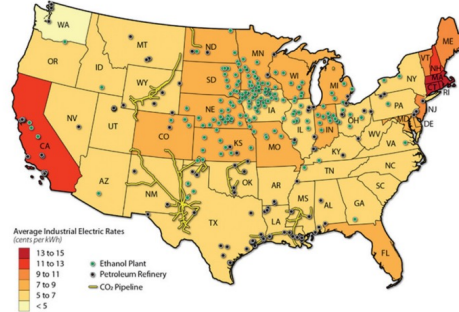
- Critical literature review and subject matter expert interviews
- Collaboration with CO₂RUE consortium members and projects

CO₂ Source



aspentech

GREET
LIFE-CYCLE MODEL



- Comparative and detailed techno-economic/life-cycle analysis coupled with point-source integration
- Risk identification and uncertainty analysis

Economic Feasibility for CO₂ Utilization Data Visualization Tool

NREL
Transforming ENERGY

Home About Conversion Pathways Price Impacts Glossary Contact Us

Bioenergy Economic Feasibility for CO₂ Utilization Data Visualization Tool Low-Temperature Electrolysis Conversion Pathway

Low-Temperature Electrolysis Conversion Pathway

Learn about the economics of producing carbon monoxide, formic acid, oxalic acid, ethylene, and ethanol from carbon dioxide (CO₂) and electricity via low-temperature electrolysis.

Low-temperature electrolysis conversion involves electrocatalytic reduction in alkaline or polymer electrolyte reactors. For each product developed using this conversion pathway, visualizations show key cost and conversion metrics based on three different cases:

- **Current** – published results in the open literature with electricity priced at \$0.068/kilowatt-hours (kWh) and a CO₂ cost of \$40/metric ton (MT)
- **Future** – attainable process improvements with electricity priced at \$0.03/kWh and a CO₂ cost of \$20/MT
- **Theoretical** – thermodynamic limitations with electricity priced at \$0.02/kWh and a CO₂ cost of \$0/MT

Select a Product and Case

Carbon Monoxide

Current Case

Future Case

Theoretical Case

Formic Acid

Oxalic Acid

Ethylene

Carbon Monoxide

Carbon monoxide is a common chemical precursor with a global production totaling ~150 million metric tons per year at an average market price of \$0.20/kg (\$0.17–\$0.26 between 2014 and 2018).

The biggest cost contributors for producing carbon monoxide from carbon dioxide and electricity via low-temperature electrolysis include capital costs and electricity feedstock cost for the current case and electricity feedstock cost for the future and theoretical cases.

Major Cost Drivers

1. Current density (mA/cm²)
2. Single-pass CO₂ conversion
3. Price of available electricity (\$/kilowatt-hour)

Minimum Selling Prices (\$2016/kg)

- Current: \$1.55
- Future: \$0.23
- Theoretical: \$0.07

- Peer-reviewed publications
- Online interactive toolkit
- Strategic roadmaps
- International consortia representation



1. Approach: FY22-FY23 Milestones

FY22 Milestones

Milestone Name/Description	Criteria	End Date
Manuscript Outline Development	Prepare outlines for manuscripts on (1) a generalized approach to integrating TEA, LCA, and uncertainty analysis and (2) a case study evaluating CO ₂ -to-ethylene technologies using integrated TEA/LCA.	12/30/2021
Establish CO₂ to SAF Process Alternatives	Establish technological alternatives to our existing SOT CO ₂ -to-SAF pathway (CO ₂ electrolysis → gas fermentation to ethanol → catalytic conversion of ethanol to SAF) and quantify reductions in cost and carbon intensity of these alternatives. This milestone is in response to risks identified in FY21 Q3 from subject matter expert interviews regarding the complexity of the existing SOT process and the commercial status of specific steps of the process (i.e., gas fermentation to ethanol).	3/31/2022
Interview Subject Matter Experts and Draft CO₂ to Fuels Strategic Plan	Using prior and new analysis combined with subject matter expert feedback, draft document summarizing opportunity space for delivering low-carbon fuels and products by 2050.	6/30/2022
Finalize Internal Draft of CO₂ to Fuels Strategic Plan	Building on efforts in Q3, finalize and submit draft of CO ₂ -to-fuels strategic plan to internal and external advisory board members for feedback.	9/30/2022

FY23 Milestones

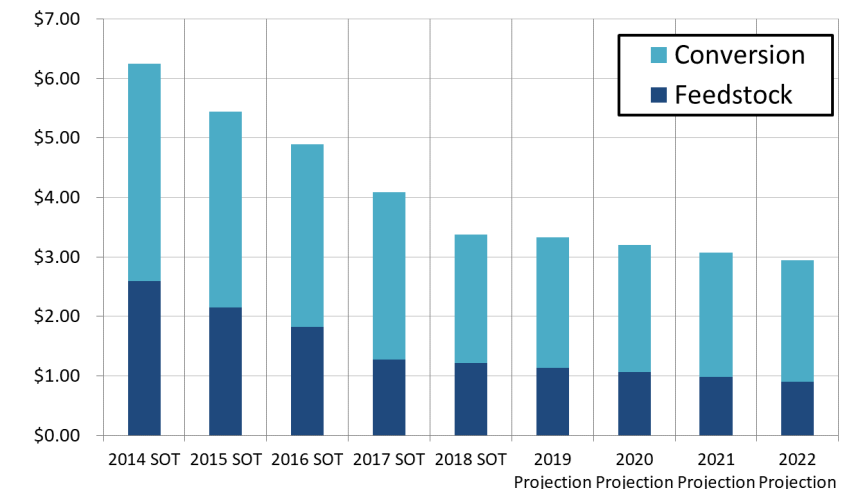
Milestone Name/Description	Criteria	End Date
Publish Strategic Plan on CO₂ to Fuels	Incorporate internal and external advisory board feedback and BETO guidance in CO ₂ to fuels strategic plan. Prepare separate manuscript for peer review journal publication capturing high-level perspectives.	12/30/2022
Update Existing TEA Models with current SOT data	Review and update existing CO ₂ -to-X process models (electrochemical, thermochemical, and biological) from our prior economic feasibility manuscript (Energy Environ. Sci., 2021, 14, 3664-3678) based on latest state of technology data.	3/31/2023
Assessment of Carbon Intensity and Life Cycle Impacts Across CO₂ Reduction Technologies	Assess the carbon intensity and life-cycle impacts for the diverse CO ₂ reduction technologies established in Q2. This work will leverage spreadsheet-based models developed in prior years to compare carbon intensity across technological approaches.	6/30/2023
Determination of TEA/LCA Trade offs for the Field of CO₂ Reduction	Integrate TEA/LCA models and determine key trade-offs for the field of electron-driven CO ₂ reduction spanning different technological approaches. This work will leverage our TEA and LCA from Q2 and Q3, respectively, and heuristics mined from the literature. This milestone will help the CO ₂ reduction field identify and understand key decision points based on TEA and LCA implications	9/30/2023



1. Approach: Analysis Methodology

Approach:

- Design conceptual process including all major steps; build model in Aspen PLUS/Excel
- **Scale basis:** CO₂ stream generated from a 90M gallon per year ethanol biorefinery
- Calculate **minimum selling price (MSP)** using discounted cash-flow analysis
- Evaluate 3 scenarios with major assumptions and technical metrics based on:
 - **SOT:** Results published in the open literature [\$0.068/kWh; \$40/tonne CO₂ cost]
 - **Future:** Attainable process improvements or engineering judgements [\$0.03/kWh; \$20/tonne CO₂ cost]
 - **Theoretical:** Thermodynamic limitations [\$0.02/kWh; \$0/tonne CO₂ cost]
- Calculate **carbon intensity (CI)** from vetted references and databases
 - GREET
 - SimaPRO Ecolnvent

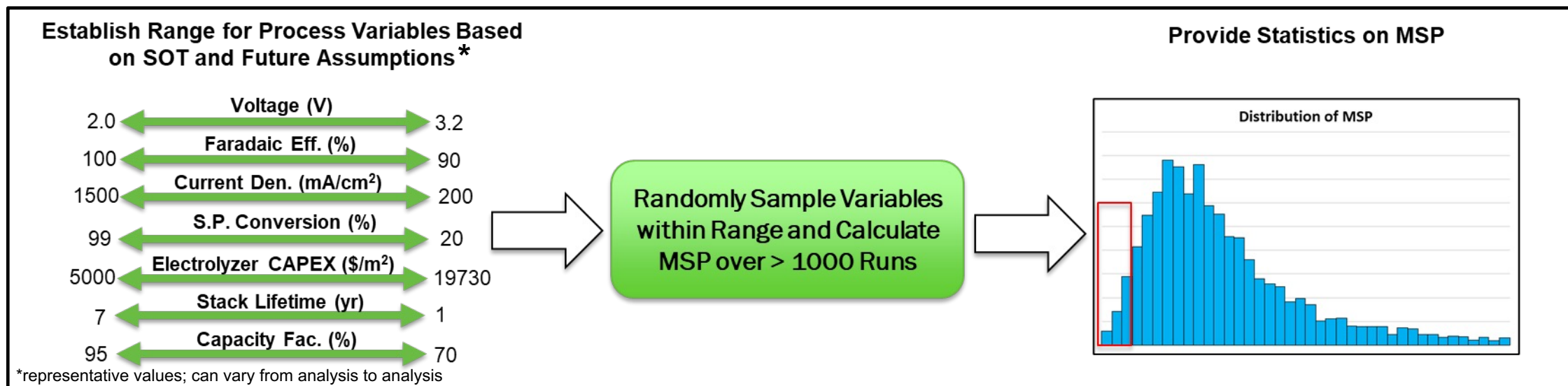


1. Approach: Analysis Methodology

Incorporating Uncertainty:

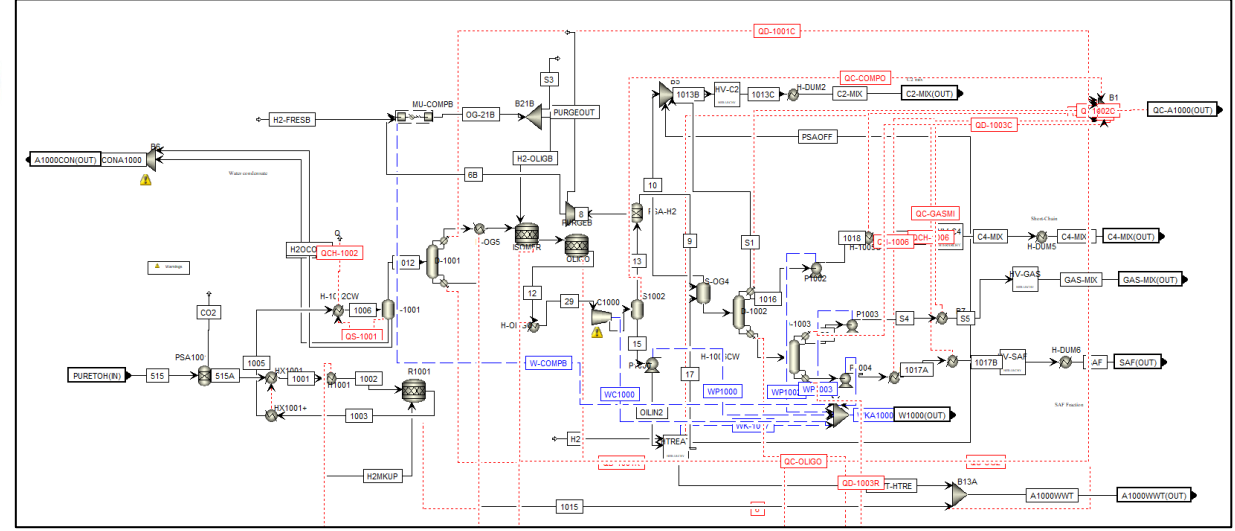
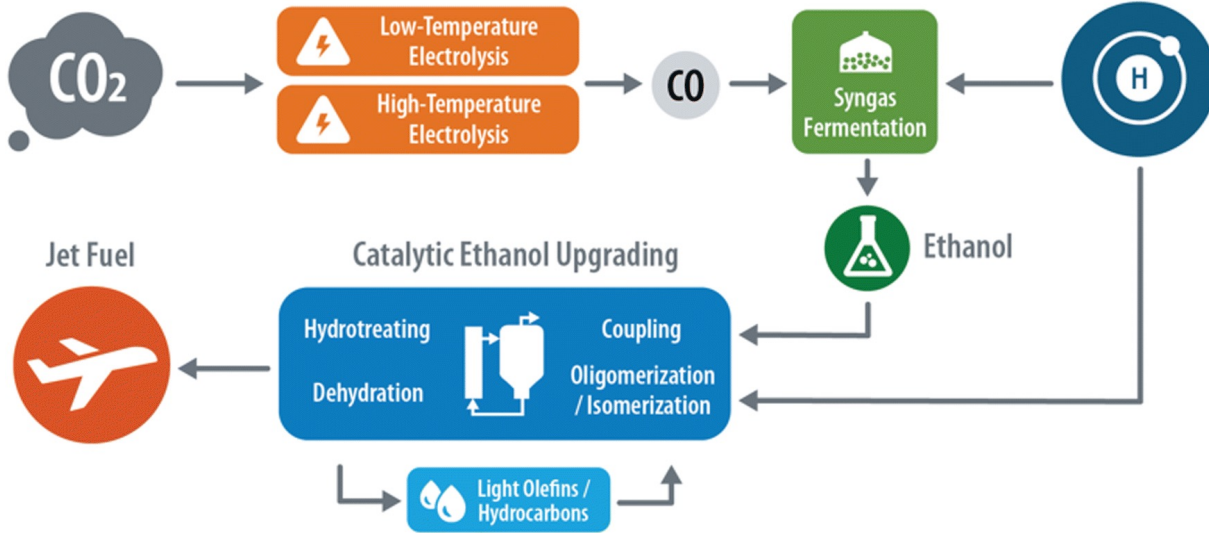
- Production cost and carbon intensity estimates often reported as single “point values”
- Significant uncertainty in input values and future assumptions often present

- **Monte Carlo Analysis** offers a pathway towards minimally-biased analysis results



MC analysis offers transparent communication of uncertainty associated with economic calculations coupled with assessment of key technical targets (red box)

2. Progress and Outcomes: Analyzing Bolt-on Tech for SAF



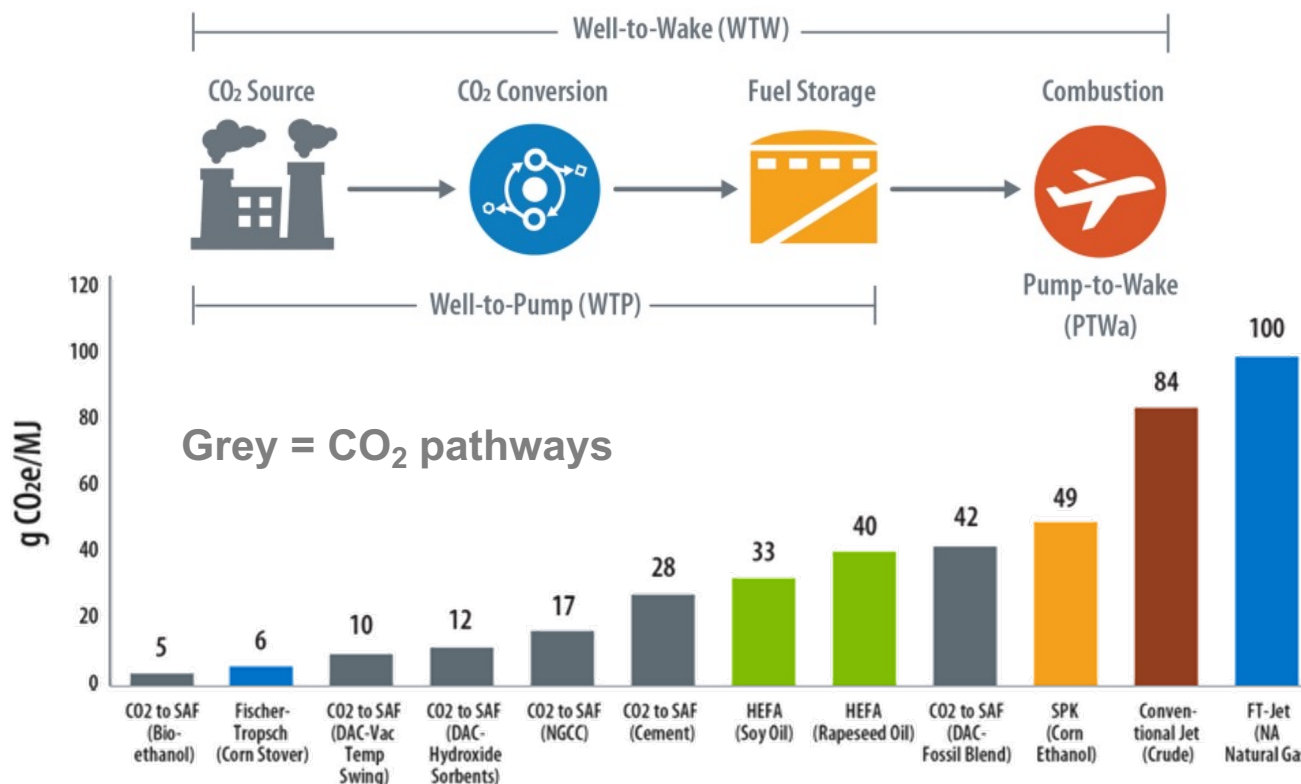
FY22 Pub: *Energy Environ. Sci.*, 2022, 15, 4798–4812

- Evaluated promising process design for a bolt-on CO₂ conversion unit for SAF
- Process design leverages core BETO strategic assets
- Near-term deployable option to reach 2030 decarbonization and SAF targets (3B gal/yr)



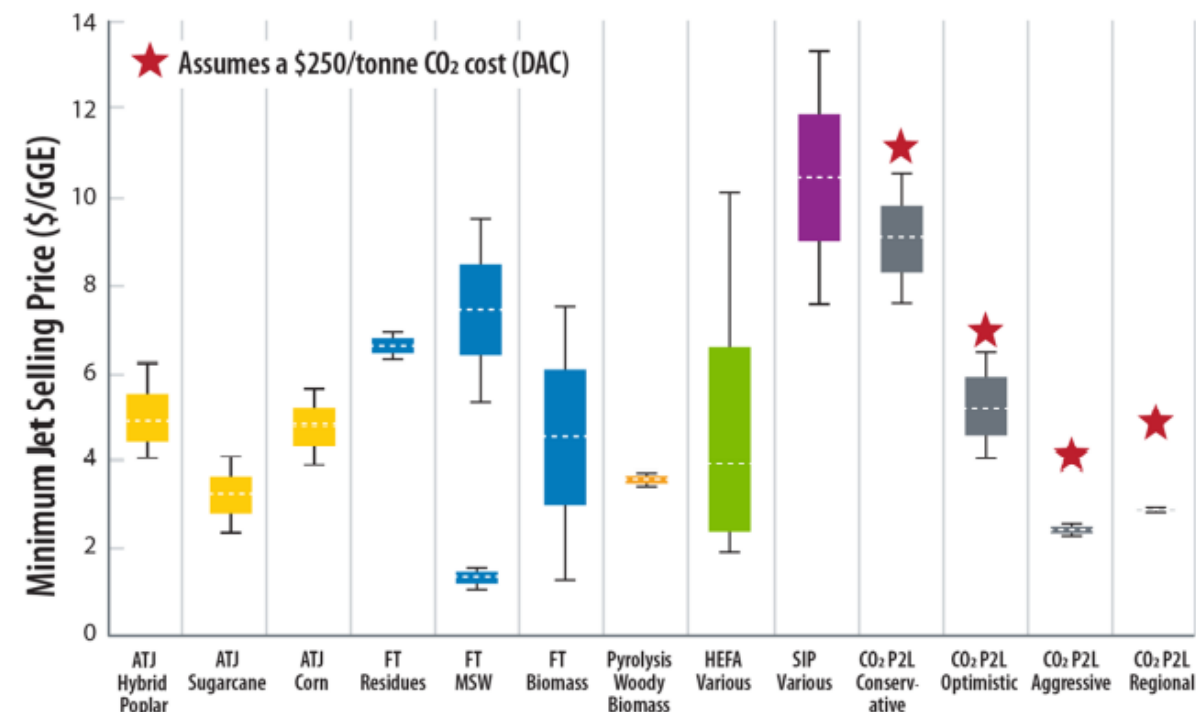
2. Progress and Outcomes: TEA/LCA for Bolt-on SAF Production

Life-cycle Analysis



Well-to-wake emissions show opportunities for 50 - 94% CI reduction relative to conventional practices

Techno-economic Analysis



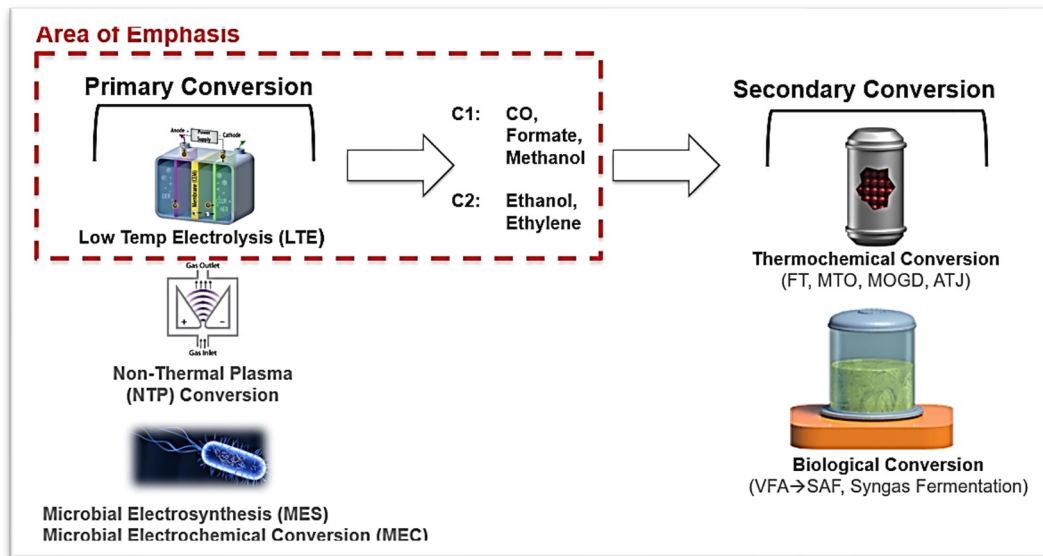
CO₂-derived SAF shows pathways to low cost with aggressive future performance and market assumptions



2. Progress and Outcomes: A Strategic Plan for CO₂ Conversion

How to drive decarbonization of fuels and chemicals by 2050?

- *Where is the “white space”?*
- *Where are the opportunities for applied R&D across low-to-moderate TRL?*
- *What are the economic and environmental targets that need to be met?*



Commercializing CO₂-based Fuels and Chemicals by 2050: R&D Gaps and Opportunities in the Direct Electrification of CO₂ Conversion

R. Gary Grim, Jack Ferrell, Zhe Huang, Ling Tao, Mike Resch

National Renewable Energy Laboratory

- *Availability of CO₂*
- *Identification of promising chemicals*
- *Strategic R&D needs*
- *Accelerated testing needs*
- *Commercialization timelines*
- *Technical targets*



2. Progress and Outcomes: Setting Future Targets

Chemical-specific Technical Targets for LTE CO₂ Conversion

	Faradaic Eff. (SOT, %)*	Faradaic Eff. (Target, %)	Current Density (SOT, mA/cm ²)*	Current Density (Target, mA/cm ²)	Voltage (SOT, V)*	Voltage (Target, V)
CO	98	95	200	1040	3.00	2.56
FA	94	95	140	850	3.50	2.59
MeOH	78	87	41.5	1075	2.67	2.57
C ₂ H ₄	60	95	1550	1045	3.23	2.59
C ₂ H ₅ OH	52	81	300	1115	2.20	2.55

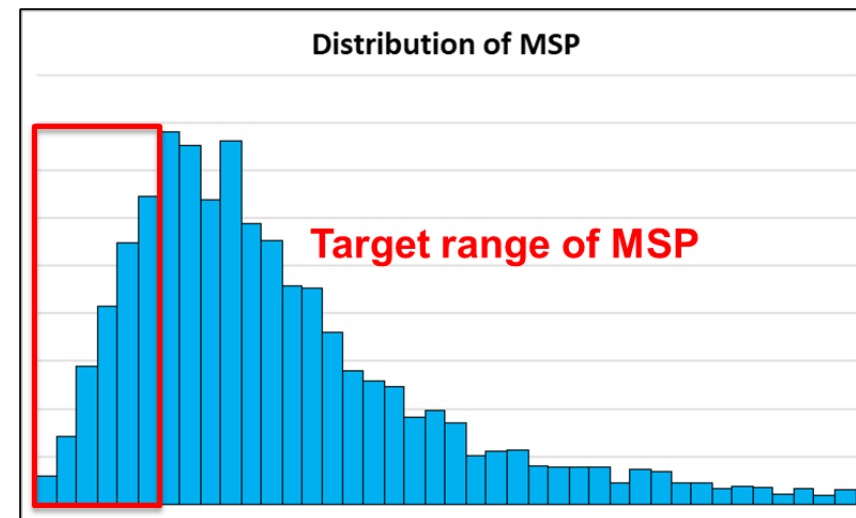
General Technical Targets for LTE CO₂ Conversion

Metric	SOT Value*	Target Value
Single Pass Conversion (%)	1 – 43	>67
Electrolyzer Unit Cost (\$/m ²)	> 19,730	< 10,600
Stack Lifetime (hours)	10 – 4,000	> 35,000
Process Capacity Factor (%)	no data	>83

*SOT = State of Technology






Target data shown assumes target product price of market +50%

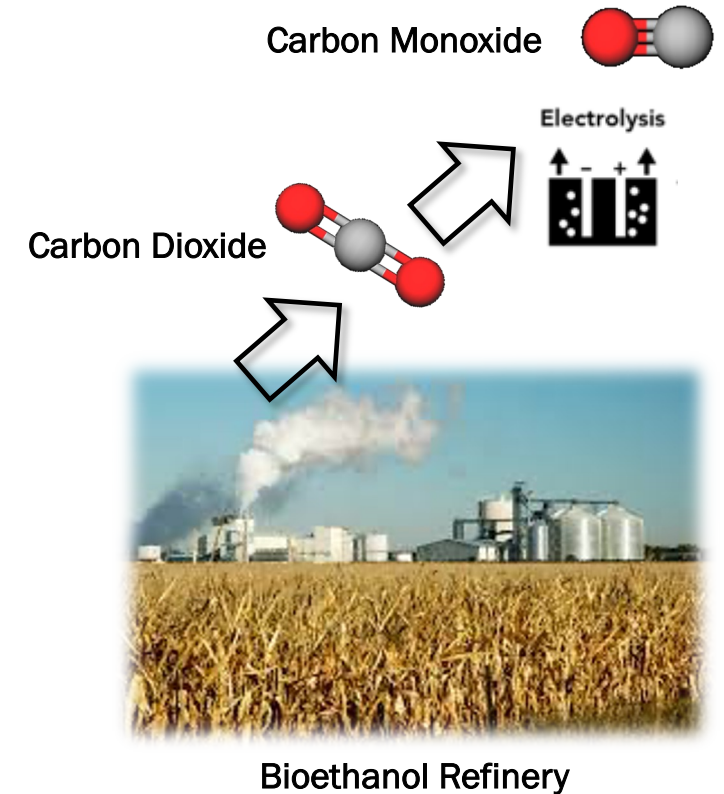
Monte Carlo analysis helps to identify specific metric by metric targets to promote an economically competitive CO₂-derived product



2. Progress and Outcomes: Theoretical Timeline for Scale Up

FY23 Pub: In Prep.

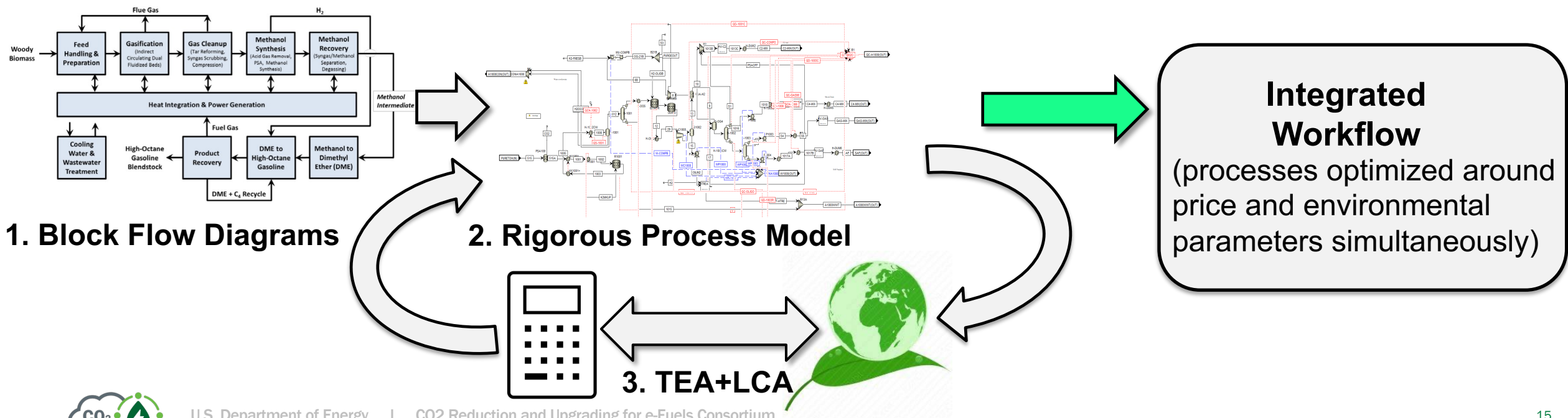
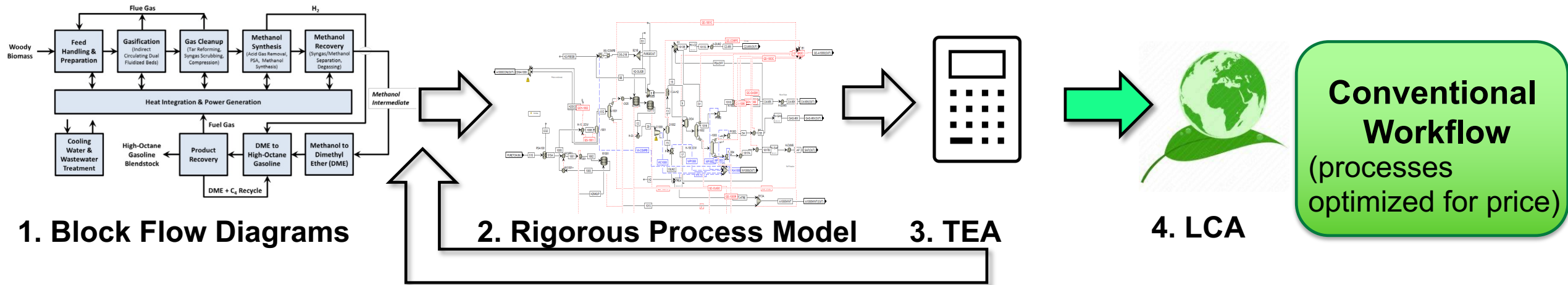
Stage				Carbon Monoxide at Bioethanol Refineries (2e-)				Technical Metrics							Target	
				Power		CO ₂ TpY	MWhe/y	Voltage (V)	FE (%)	CD (mA/cm2)	Conv. (%)	Unit Cost (\$/m2)	Stack Lifetime (hr)	Capacity Factor (%)	Year	
			Commercial 	110	MWe	266,500	820,000	2.56	95	1,040	71	\$11,175	35,040	83	2050	
				20	MWe	53,300	164,000	2.63	95	950	71	\$12,092	31,693	77	2047	
				4	MWe	10,660	32,800	2.70	96	860	71	\$13,008	28,346	72	2044	
		Pilot 		1	MWe	2,665	2,050	2.77	96	770	71	\$13,925	24,999	66	2041	
	Scaling/ Reliability 			250	kWe	666	410	2.83	96	680	71	\$14,841	21,651	60	2038	
				50	kWe	133	82	2.90	97	590	59	\$15,758	18,304	55	2035	
				10	kWe	27	8	3.02	97	440	38	\$17,286	12,726	45	2030	
Concept/ Research 				1	kWe	3		3.13	98	290	17	\$18,813	7,147	36	2025	
				100	W			3.2	98	200	5	\$19,730	3,800	30	2022	
				10	W										2020	
				1	W										2014	



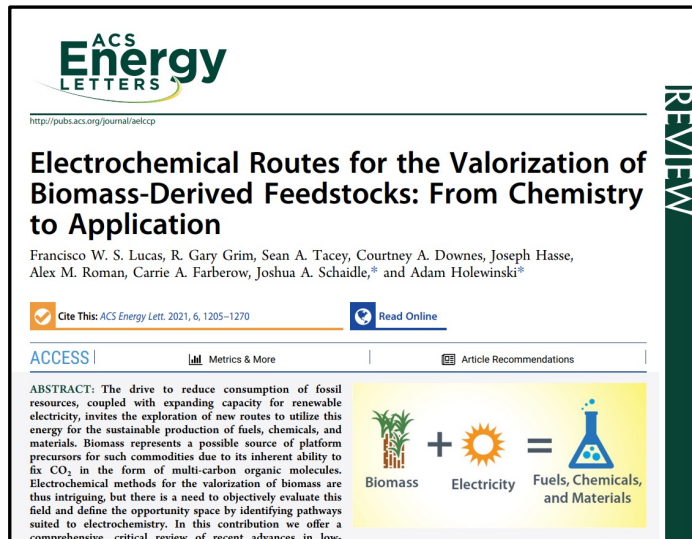
Reaching technical targets and commercializing CO₂-derived products *from direct electrification potentially* achievable by 2050 with sustained gains in metrics as outlined, informed by historical precedents in the PEM H₂O electrolysis industry



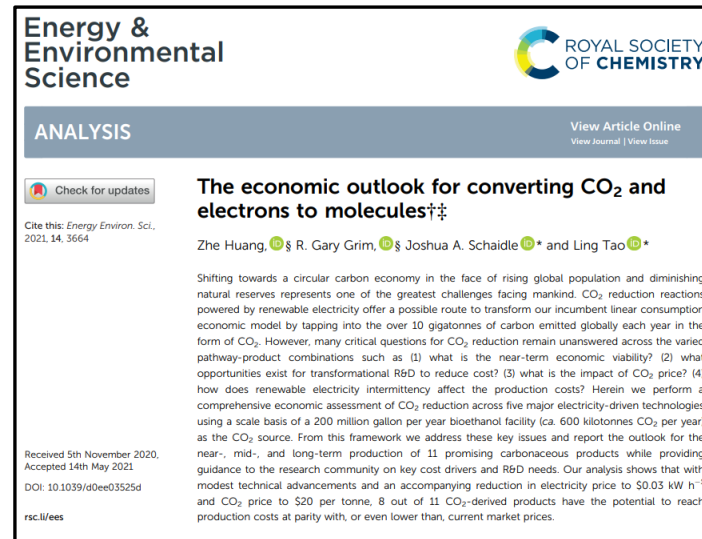
2. Progress and Outcomes: Integrated TEA/LCA



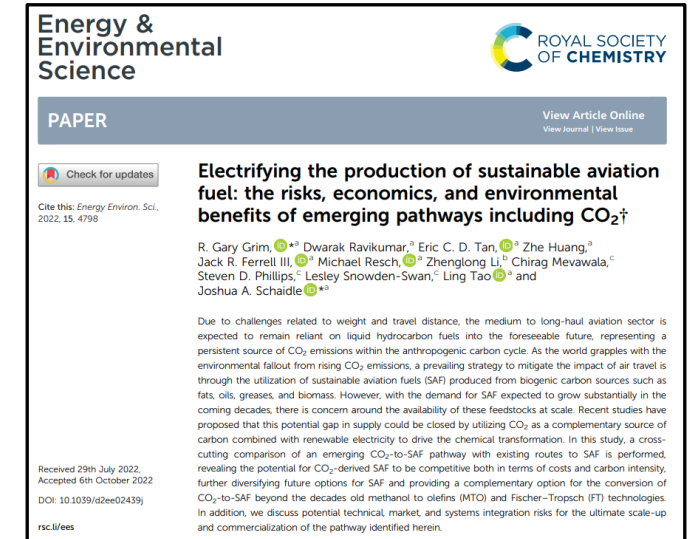
3. Impact: Peer-reviewed Publications



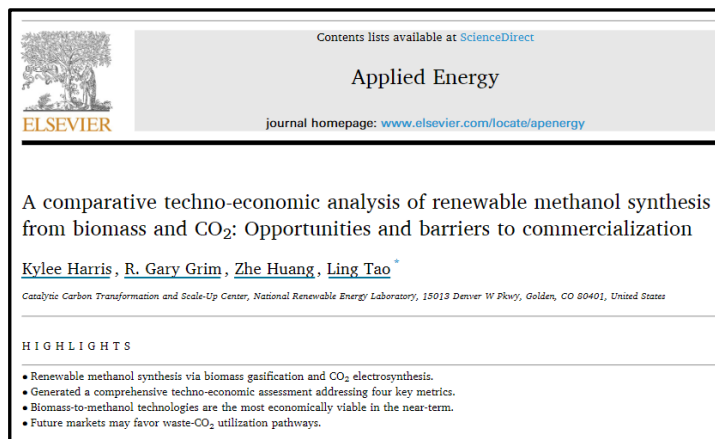
ACS Energy Lett. 2021, 6, 4, 1205–1270 **Impact Factor: 23.1**



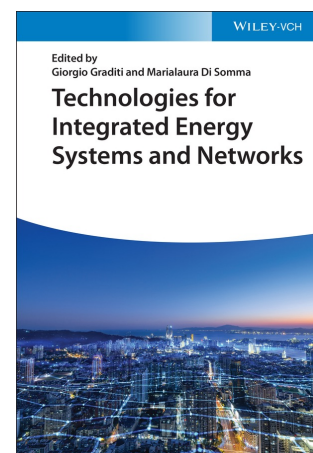
Energy Environ. Sci., 2021, **14**, 3664–3678 **Impact Factor: 38.5**



Energy Environ. Sci., 2022, **15**, 4798–4812 **Impact Factor: 38.5**



Appl. Energy. 2021, 303, 117637 **Impact Factor: 9.7**



3 Power Conversion Technologies: The Advent of Power-to-Gas, Power-to-Liquid, and Power-to-Heat

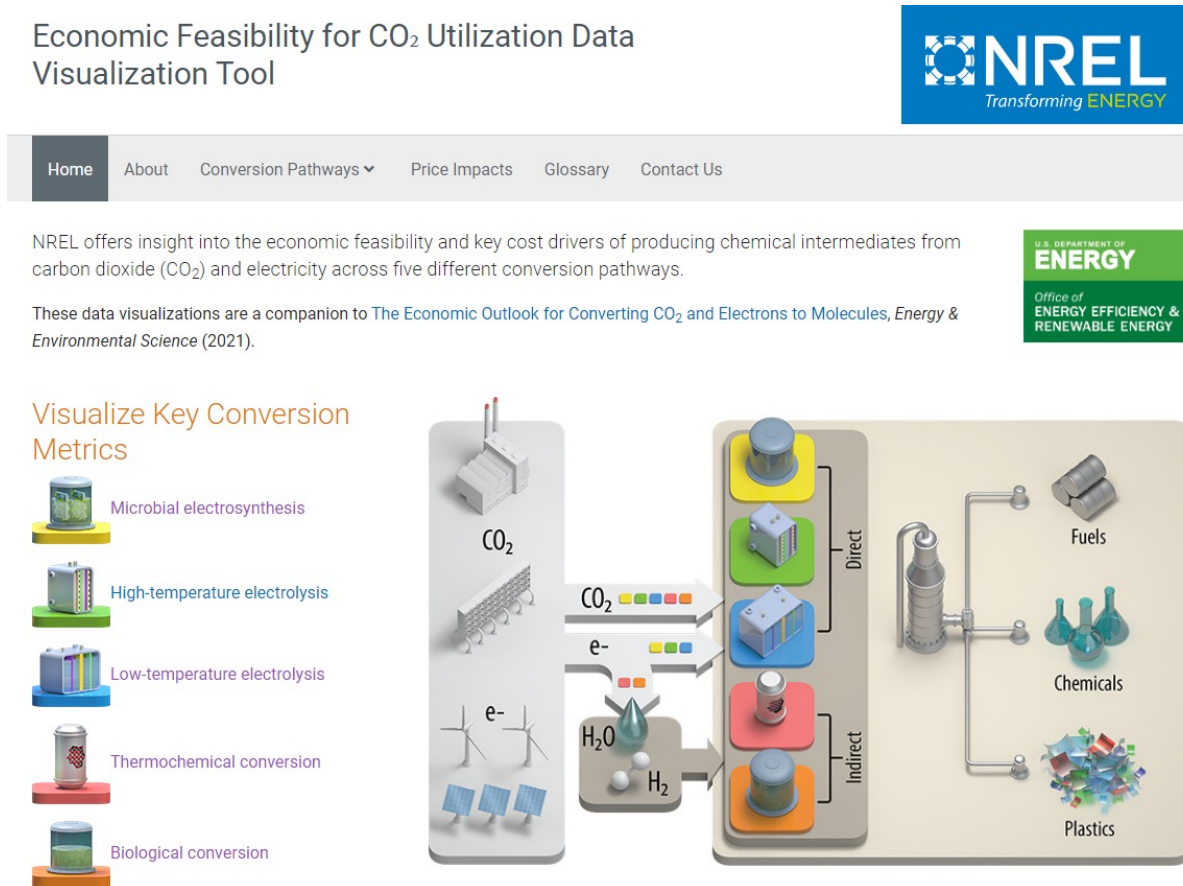
Joshua A. Schaidle, R. Gary Grim, Ling Tao, Mark Ruth, Kevin Harrison, Nancy Dowe, Colin McMillan, Shanti Pless, and Douglas J. Arent
National Renewable Energy Laboratory, 15013 Denver West Parkway, Golden, CO, 80401, USA

March 2022
doi.org/10.1002/9783527833634.ch3

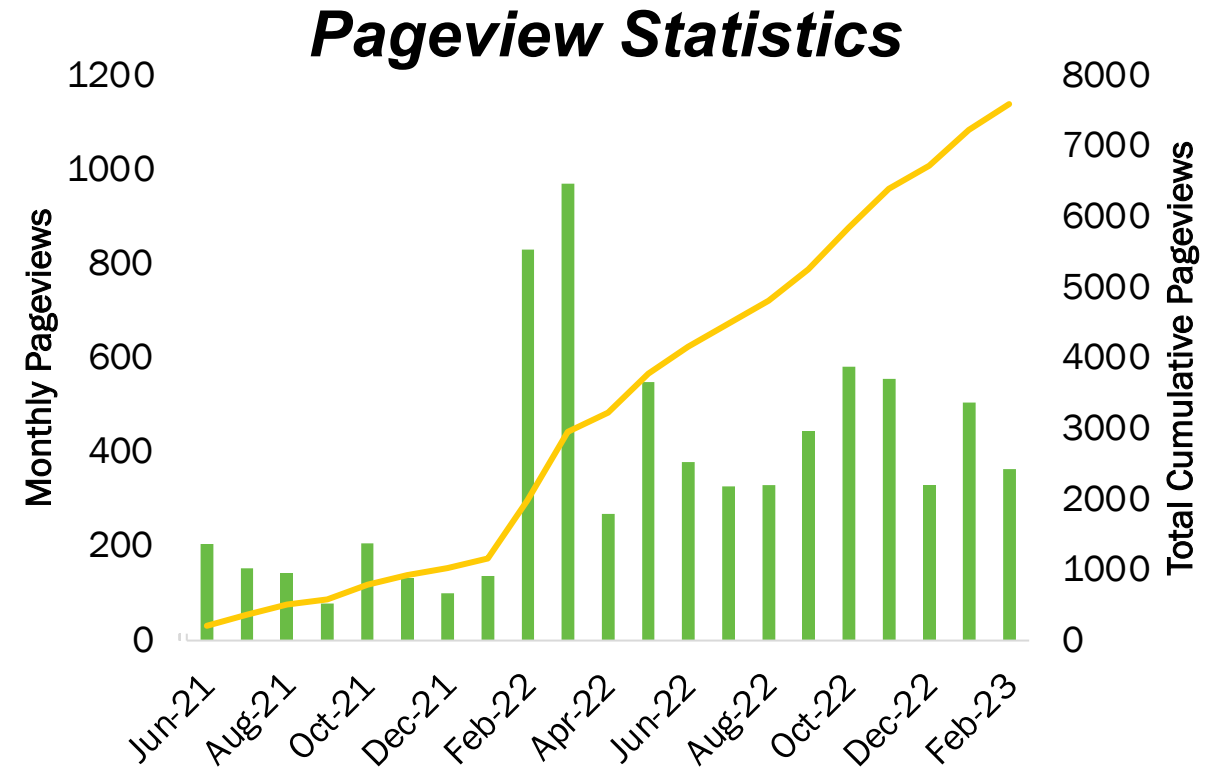
5 publications + internal technical reports delivered since previous peer-review meeting



3. Impact: *Interactive Website*



<https://www.nrel.gov/bioenergy/co2-utilization-economics/>



Positive reactions and increased engagement across a wide variety of users: industry (SpaceX), VC firms, academia, national laboratories

Summary

Goal: *Guide existing and future R&D* efforts by defining key technical challenges, risks, cost/carbon intensity drivers, and future technical targets for utilizing renewable electricity and CO₂ to accelerate and drive industrial decarbonization and CO₂ conversion

Approach and Progress: Connecting key technical challenges and risks with impacts on cost and carbon intensity as a means to *provide actionable information* to R&D teams within BETO, the CO₂RUE consortium, and the broader scientific and industrial communities

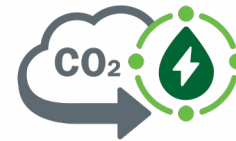
Outcomes: (1) FY21 – Analyzed promising *bolt-on compatible CO₂ reduction pathways* to fuels or products from standalone biorefineries, (2) FY22 – Published a *comprehensive strategic plan* for achieving industrial decarbonization goals via CO₂ conversion, with inclusion of outyear technical, cost, and carbon intensity targets, and (3) FY23 – Developing methods for *integrated TEA/LCA*

Relevance to Bioenergy Industry: Identify risks and opportunities for leveraging low-cost electricity to improve biorefinery carbon utilization. Identify specific and actionable technical metrics to advance the deployment of technologies



Thank You

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**CO₂ Reduction and Upgrading
for e-Fuels Consortium**

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